



Scale and corrosion inhibition in the Netherlands and France

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Geofluid

1. Corrosion and scaling issues
2. Scaling and Corrosion in Paris Basin
3. Scaling and corrosion issues in the NL
4. Scaling and corrosion issues in the NL
5. Guidelines

## Corrosion and scaling issues

- General (uniform) corrosion
- Pitting corrosion
- Crevice corrosion
- Underdeposit corrosion
- Galvanic corrosion
- Impingement
- Stress corrosion cracking (SCC)
- Erosion
- Corrosion by microbacteria



	Average Corrosion Rate		Maximum Pitting Rate (See Paragraph 2.5)	
	mm/y <sup>(A)</sup>	mpy <sup>(B)</sup>	mm/y	mpy
<b>Low</b>	<0.025	<1.0	<0.13	<5.0
<b>Moderate</b>	0.025-0.12	1.0-4.9	0.13-0.20	5.0-7.9
<b>High</b>	0.13-0.25	5.0-10	0.21-0.38	8.0-15
<b>Severe</b>	>0.25	>10	>0.38	>15

<sup>(A)</sup> mm/y = millimeters per year

<sup>(B)</sup> mpy = mils per year

## Corrosion and scaling issues

### Precipitation (deposition of solids)

Earth Energy (Geothermal Heat Pumps)	
Component	Examples
Calcium carbonate	•Various sites
Iron oxides	•Various sites
Low and medium-enthalpy fluids	
Component	Examples
Calcium carbonate	•Oradea and Ciuneghia (Romania), Balçova (Turkey), Saidene (Tunisia) N. Kessani and Nigrita (Greece),
Iron oxides	•Nigrita (Greece)
Iron sulphide salts [in association with corrosion]	•Dogger Basin (France)
High-enthalpy fluids	
Component	Examples
Calcium carbonate	•Kizildere (Turkey), Miravalles (Costarika), Lartera (Italy), Cerro Prieto (Mexico), East Mesa, Nevada (USA), Krafla (Iceland)
Silica (and metal-silicates) [usually associated with small or medium TDS]	•Svartsengi and Nesjavellir (Iceland), Dixie Valley (USA), Matsukawa, Otake and Onuma (Japan), Berlin (El Salvador)
•Heavy metal sulphide salts (with silica and metal-silicates) [associated with high TDS]	•Salton Sea (USA), Milos Island (Greece), Asal Wells (Djibouti)
•Copper (and other heavy metal)	•Buckingham (USA)

## Corrosion and scaling issues

	<i>Salton Sea, California</i>	<i>Broadlands 1, N. Zealand</i>	<i>Hot Springs, Utah</i>	<i>Kilauea, Hawaii</i>	<i>Krafla, Iceland</i>	<i>Kizildere (W15), Turkey</i>	<i>Klamath Falls, Oregon</i>	<i>Dogger, Paris Basin, France</i>	<i>Nigrita, Greece</i>	<i>Pijnacker, The Netherlands</i>
pH	5.7	8.3	-	7.1	7.2	8.0	8.4	6.2	6.8	5.9
Temp., °C	214	270	260	190	220	138	80	73	59	80
TDS (g/L)	182	3.8	7.4	15.8	1.0	2.4	0.7	15	2.5	101
Na	42700	1060	2320	4930	193	1192	205	3700	529	38150
K	6500	150	461	756	20	135	4.3	60	89	230
Ca	18200	5	8	358	1.5	1.9	26	630	160	4900
Mg	570	0	2	0.3	0.03	0.2	0.5	150	105	860
Fe	180	0.2	1	0	0.02	0	0.3	0.5	1.1	39
Pb	59	-	-	0	0	-	-	-	-	<1
Cl	112000	1700	3860	8970	26	46	51	7980	162	69850
SO <sub>4</sub> <sup>2-</sup>	6	40	72	24	194	631	330	775	130	13
HCO <sub>3</sub> <sup>-</sup>	220	300	232	18	328	-	35	335	2200	
As	22	5	4	0.1	-	-	-	-	0.5	
B	480	7	-	4.3	-	24	-	5	4.6	30
SiO <sub>2</sub>	1150	600	563	750	383	356	48	14	38	12

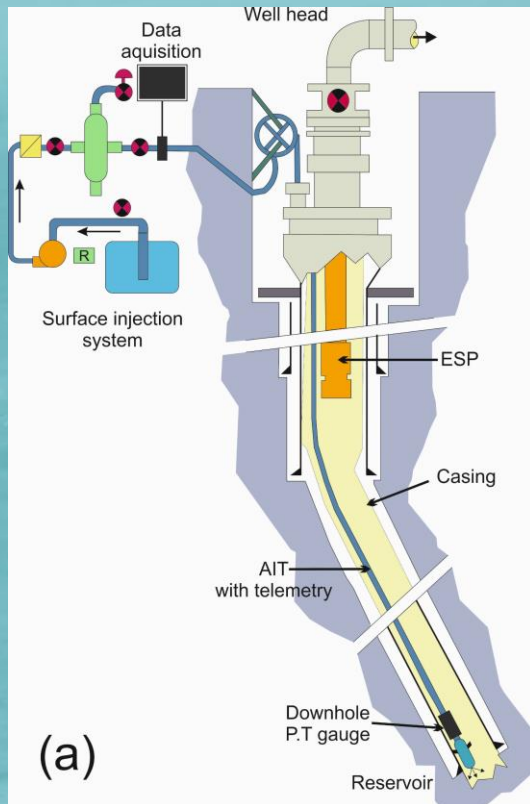


## Scaling and corrosion in Paris basin

Conditions	Corrosion issues	Scaling issues
TDS ~ 15 g/l	Harsh (sour) conditions → Film forming amines injected	Mostly Pyrite ( $\text{FeS}_2$ ) formation due to enhanced [Fe] concentration by corrosion
[Fe] = 0.5 mg/l	Sulphide reducing bacteria → biocide injection	
$\text{CO}_2$ and $\text{H}_2\text{S}$ → Sour		
T = 65-90 °C		
Bubble point ~3-10 bar		

Corrosion causes [Fe] increase, and thus results in pyrite scale formation  
→ Corrosion control is of utmost important

# Scaling and corrosion in Paris basin



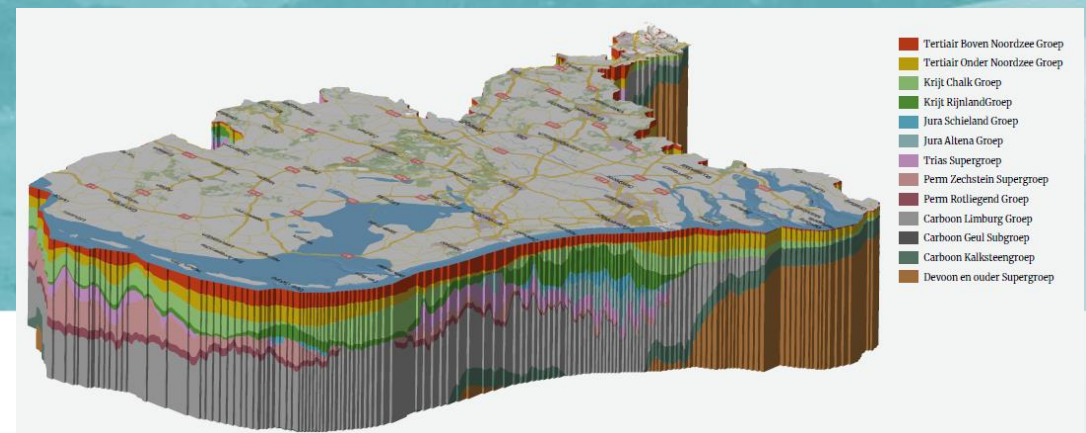
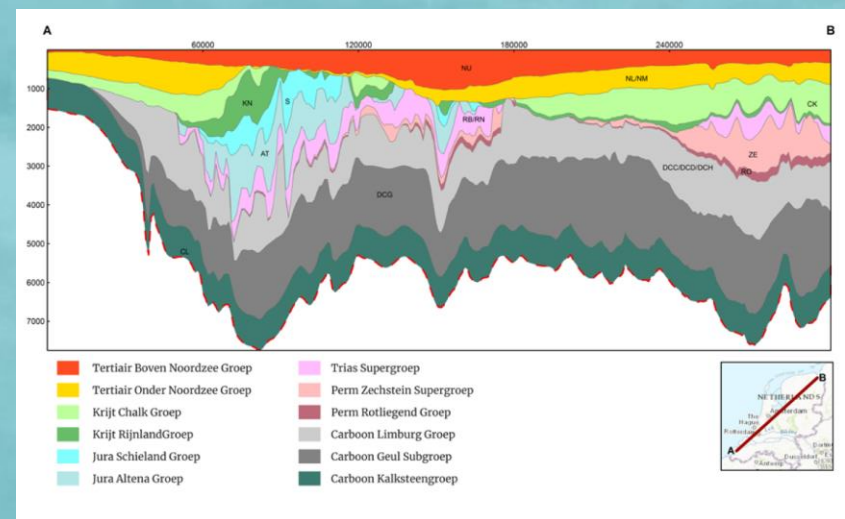
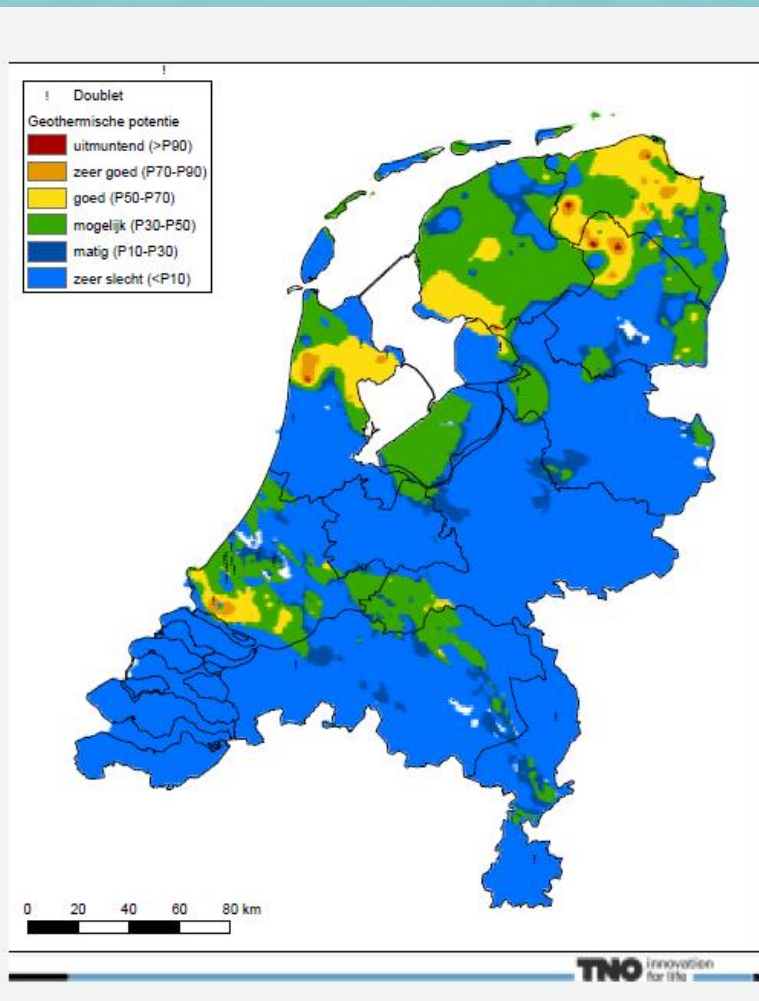
(a)

AIT line (propriety GPC)





# Scaling and corrosion in Netherlands



## Scaling and corrosion in Netherlands

So far, geothermal energy is mostly developed by greenhouse owners



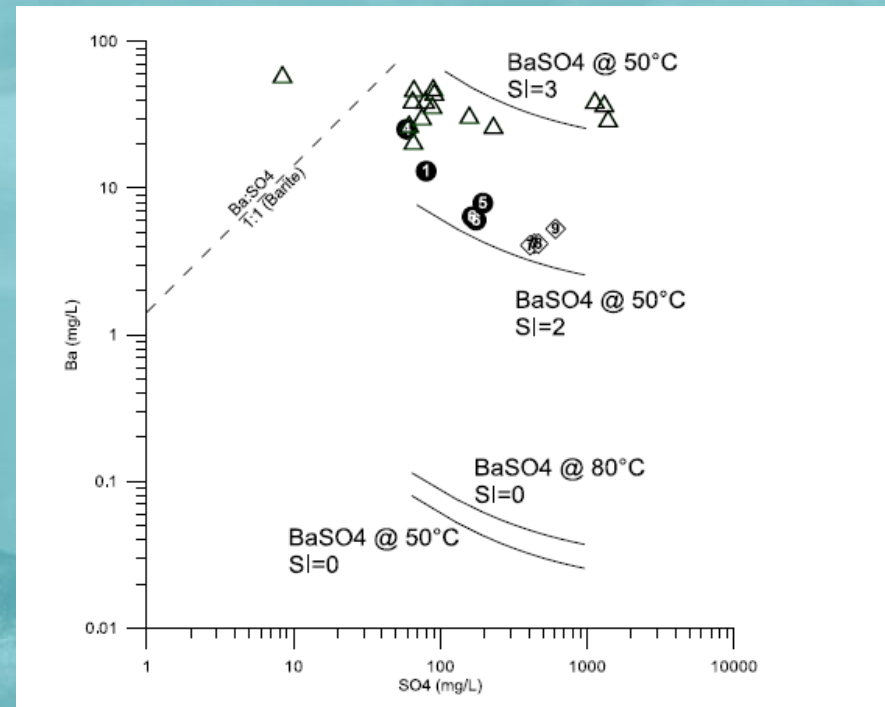
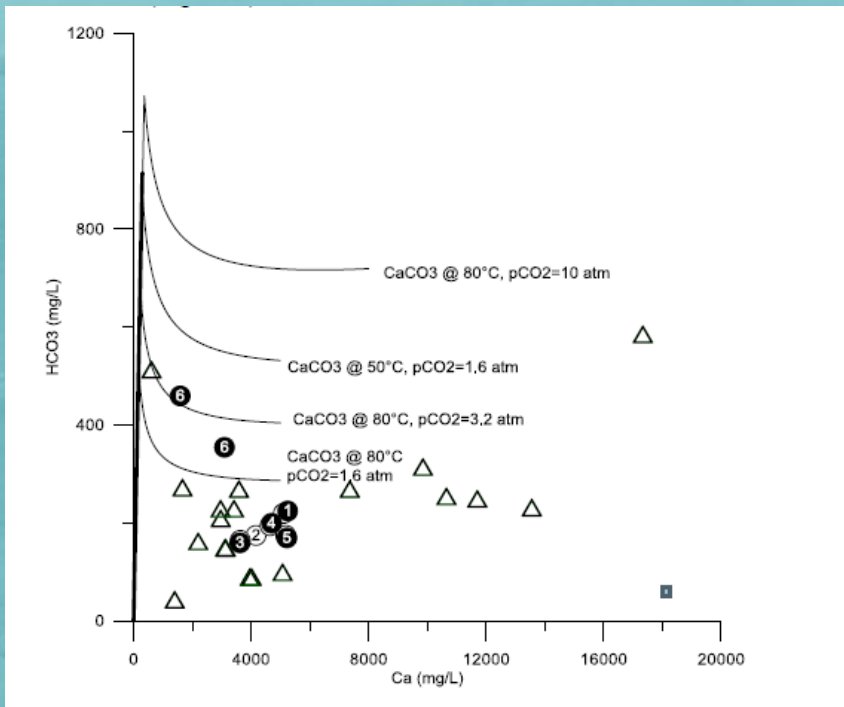
## Scaling and corrosion in Netherlands

Conditions	Corrosion issues	Scaling issues
TDS ~110 g/l	Galvanic corrosion in early wells	Mostly calcite and siderite deposition
[Fe] =30 mg/l Traces Pb	Pitting corrosion?	→ increase pressure in surface installation
Gas composition is mainly CH <sub>4</sub> , N <sub>2</sub> , CO <sub>2</sub>	Erosion (cavitation) of couplings	
T = 80-100 °C	Pb deposition	
Traces of oil, aromatics		
Bubble point ~20-40 bar		

## Scaling and corrosion in Netherlands



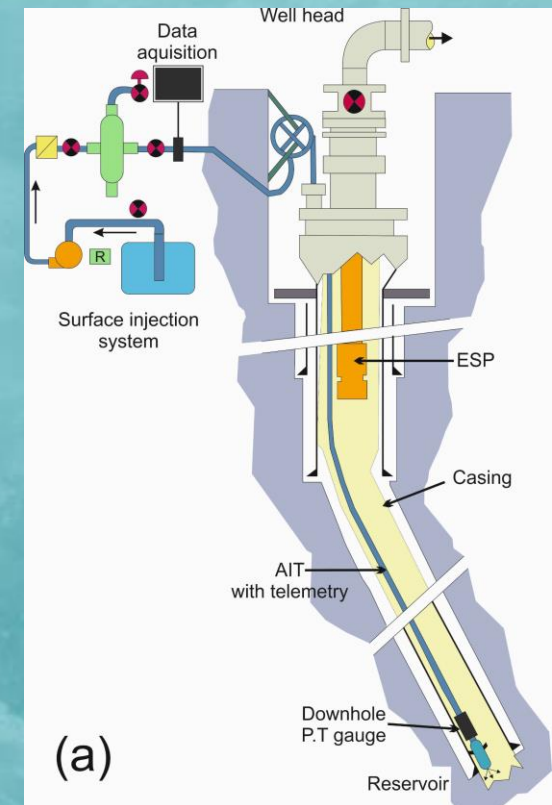
# Scaling and corrosion in Netherlands



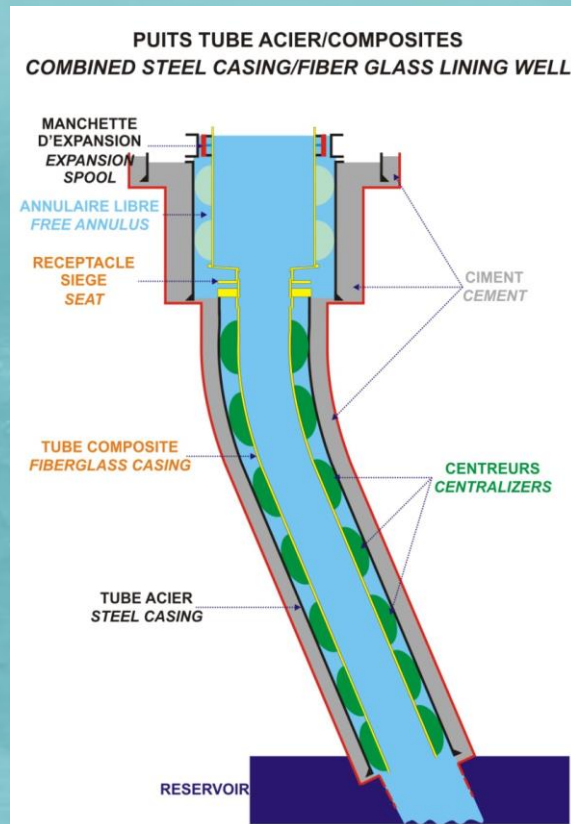
## How to mitigate corrosion and scaling

### ***Corrosion mitigation***

- Use suitable corrosion inhibitors (filming amines)
  - Test efficiency of products
  - Monitor corrosion rate
- Inject inhibitor downhole
- Option: Use GRE liners
- Option: Use high steel grades



## How to mitigate corrosion and scaling



Patent GPC



Installation in Bonneuil

## How to mitigate corrosion and scaling

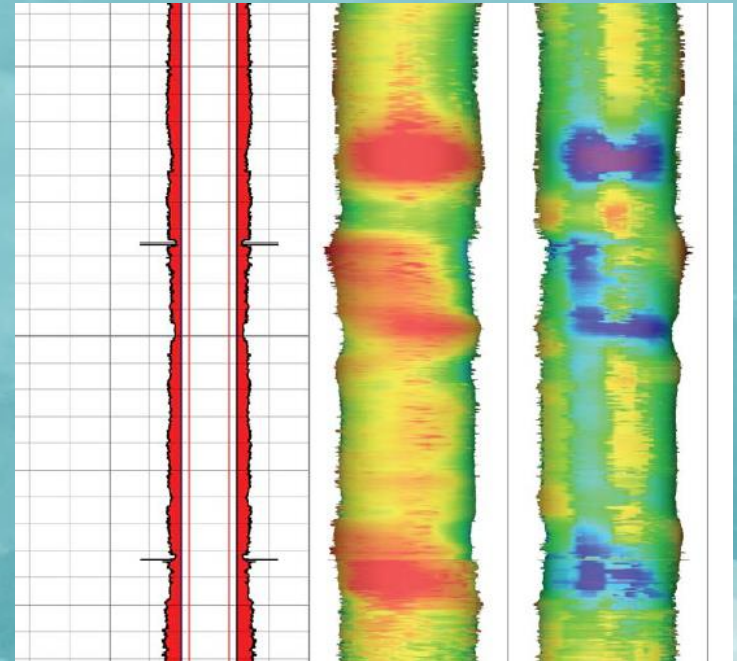
### *Scaling mitigation*

- Estimate scaling risks (e.g PHREEQC)
- Determine minimum injection temperature in injection well
- Prevent CO<sub>2</sub> degassing
- Inject inhibitor product
  - Carbonate scale deposition at depth
  - Most other scales (e.g. sulfate, silicate) at surface before HX



## Monitoring

Corrosion Monitoring	Accuracy
Well logging	+++
Coupons analysis	++
Iron content	++
Corrator (LPR)	~
Test kits	++



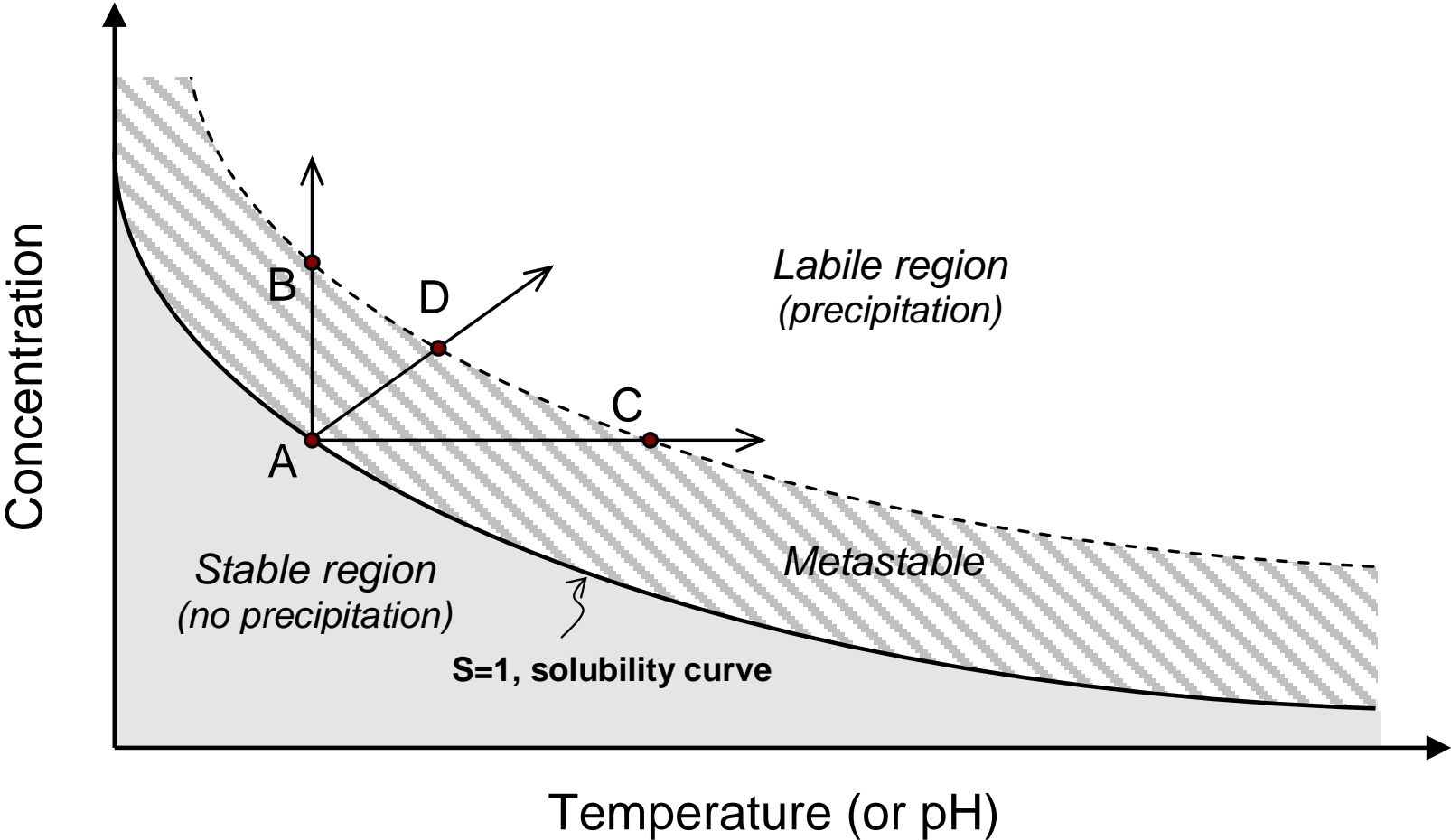
## Monitoring

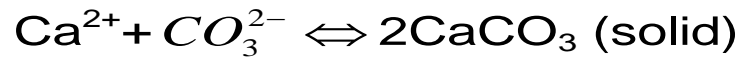
Scale monitoring	Accuracy
Well logging	+++
Coupons analysis	++
Deposit analysis (XRF, XRD, SEM,....)	++
Corrator (LPR)	~
Monitor ionic concentrations	++
Measure chemical parameters (pH, ...)	+
Monitor particle concentration	+





# SCALING SOLUBILITY. SUPERSATURATION DIAGRAM





Langelier-Saturation-Index (LSI)

$$\text{LSI} = \text{pH} - \text{pH}_s$$

$$\text{pH}_s = (9.3 + A + B) - (C + D)$$

where :

$$A = [\log(\text{TDS}) - 1] / 10$$

$$B = -13,12 \times \log \theta + 34,55$$

$$C = \log[\text{Ca}^{2+}] - 0,4$$

$$D = \log [\text{alkalinity}]$$

TDS in mg/L

$\theta$ , temperature in K

$\text{Ca}^{2+}$  as mg/L  $\text{CaCO}_3$

alkalinity as mg/L  $\text{CaCO}_3$